SYNTHESIS OF ZEOLITE-A FROM PUMICE SILICA AND ALUMUNIUM FOIL AS A CATALYST FOR PYROLYSIS OF PALM OIL MILL EFFLUENT (POME)

(Skripsi)

By

QUNTUM RAMADHINA



FACULTY OF MATHEMATICS AND NATURAL SCIENCES LAMPUNG UNIVERSITY BANDAR LAMPUNG 2023

ABSTRACT

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In this research, palm oil mill effluent (POME) was converted into liquid fuel by pyrolysis method using zeolite-A as a catalyst with various calcination temperature, to study the effect of it towards the characteristic of liquid fuel. Zeolite-A was synthesized from pumice silica and food grade aluminium foil with hydrothermal method at 100°C for 72 hours, then calcined at 600, 700, and 800°C for 6 hours. Synthesized zeolite-A was then characterized using XRD and SEM to ensure the formation of zeolite-A. Liquid fuel produced from the catalytic upgrading process using zeolite-A was analyzed using GC-MS to identify the components contained in the sample. The GC-MS results show the most optimum catalyst used for catalytic upgrading in terms of hydrocarbon was zeolite-A 800°C with relative percentage of 81.37%. In terms of hydrocarbon chain in range of bio gasoline, zeolite-A 700°C with relative percentage of 81.37%.

Keywords: Palm oil mill effluent, liquid fuel, pyrolysis, zeolite-A, synthesized, pumice.

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By

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SINTESIS ZEOLIT-A DARI SILICA BATU APUNG DAN ALUMINIUM FOIL SEBAGAI KATALIS PIROLISIS *PALM OIL MILL EFFLUENT* (POME)

Oleh

QUNTUM RAMADHINA

Skripsi

Sebagai salah satu syarat untuk memperoleh gelar Sarjana Sains

pada

Jurusan Kimia Fakultas Matematika dan Ilmu Pengetahuan Alam



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Menyatakan bahwa skripsi yang berjudul "Synthesis of Zeolite-A from Pumice Silica and Aluminium Foil As A Catalyst for Pyrolysis of Palm Oil Mill Effluent (POME)" adalah benar hasil karya sendiri dan tidak pernah menggunakan dan diterima sebagai syarat penyelesaian studi pada universitas lain. Saya tidak keberatan jika data dalam skripsi ini digunakan oleh dosen atau program studi untuk kepentingan publikasi sesuai kesepakatan.

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RIWAYAT HIDUP

Penulis bernama lengkap Quntum Ramadhina, lahir di Tangerang pada 15 Desember 2001 dan merupakan anak ke-2 dari 3 bersaudara, dari pasangan suami istri Bapak Jerry Sonya Putra dan Ibu Tuti Yuliani.

Penulis menyelesaikan pendidikan mulai dari Taman Pendidikan Al-Qur'an (2005 – 2006), SD Negeri Bojongnangka (2006 – 2012), SMP Negeri 2 Kelapa Dua (2013 - 2016), SMA Negeri 23 Kabupaten Tangerang (2016 – 2019), dan mulai tahun 2019 hingga penulisan skripsi ini, penulis melanjutkan ke Perguruan Tinggi Negeri di Jurusan S1 Kimia FMIPA Universitas Lampung melalui jalur SBMPTN.

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"I don't chase, I attract. What belongs to me will simply find me"

"When life deals us card, make everything taste like it is salt" – Ariana Grande Buttera

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I. INTRODUCTION

1.1. Background

Sustainability of energy is a global concern, which remain as prime energy sources, not renewable and their natural deposit is continuously depleted due to massive exploration. In addition, fossil fuels are the main sources of greenhouse gases and causing many environmental and health problems associated with global warming. Hence, the development of renewable and more environmental friendly energy sources in order to reduce the reliance on fossil fuels is crucially needed. In this respect, continuously growing interests have been focussed on the development of biomass derived energy sources, generally known as biofuel.

At present, three types of liquid biofuel produced by pyrolysis of biomass, *i.e.* bioethanol, biodiesel, and bio crude oil (BCO) are continuously explored. Bioethanol is a product of fermentation of reducing sugars, such as glucose. The advantages of using bioethanol as biofuel includes; high octane number, higher heat of vaporization, low boiling point, and comparable energy content. However, bioethanol also has disadvantages, such as lower energy density compared to gasoline, corrosive, miscibility with water, and lower vapour pressure .

Biodiesel is a renewable and biodegradable fuel produced from vegetable oils, animal fats, or waste cooking oil. Biodiesel can be obtained by transesterification process using simple alcohol, primarily methanol, to convert glycerides in fats and oils into their corresponding methyl esters, and glycerol. Biodiesel has been used as practical fuel by mixing with petrochemical fuel at certain portions such as B20 (Bari., 2014), B30 and B40 (Pramudito *et al.*, 2022).

However, biodiesel also has some drawbacks, such as more expensive than petrochemical diesel, not suitable to be used in low temperatures, and clogging in engine.

Bio crude oil (BCO) is a liquid biofuel produced by pyrolysis of biomass. Pyrolysis is a heating process of biomass in a tightly closed reactor at high temperature, leading to degradation of large organic molecules into smaller products, which consist of uncondensed gases, BCO, and residual solid.

From energy source point of view, BCO is the most valuable product of biomass pyrolysis, and therefore this particular product has become a focus of extensive studies. Chemically, BCO is a complex mixture of a large number and different types of organic compounds, such as hydrocarbon, ketone, acid, alcohol, and ester (Simanjuntak *et al.*, 2019). The composition of BCO is determined by several factors, in raw materials and catalysts are the most significant factors. Variation in chemical composition of BCO is evidently reflected by the results of previous studies on pyrolysis of different feedstocks, such as cassava solid waste (Simanjuntak *et al.*, 2019), poultry litter and hardwood (Agblevor *et al.*, 2010), sugar cane bagasse (Simanjuntak *et al.*, 2017), palm oil (Febriyanti *et al.*, 2021), torrefied of cassava root and palm oil (Simanjuntak *et al.*, 2021), and coffee grounds (Bok *et al.*, 2012). Although the formation of common substances should also be acknowledged.

The catalyst is another important element in biomass pyrolysis, not only to lower the temperature, as a general function of catalyst, but also to determine the composition of product. Considering these important roles, various types of catalyst have been developed, such as aluminium metal (Simanjuntak *et al.*, 2017), zeolite-Y (Supriyanto *et al.*, 2018), zeolite ZSM-5 (Yang *et al.*, 2004), zeolite-X (Pandiangan *et al.*, 2017), zeolite-A (Simanjuntak *et al.*, 2021), and mordenite (Li *et al.*, 2009). Among various types of catalysts, zeolite is the most widely used because of the deoxygenation ability, stable at high temperature, and non-toxic.

Due to its advantages, synthetic zeolites have been developed and zeolite-A is one of those included. In this research, zeolite-A was synthesized from pumice silica and food grade aluminium foil as a catalyst of pyrolysis of POME.

1.2. Research Purposes

The purpose of this research is as follows :

- 1. To obtain amorphous pumice silica extracted with sol gel method.
- 2. To obtain zeolite-A from pumice silica and food grade aluminium foil with hydrothermal method.
- 3. To obtain data about the characteristics of pumice silica including crystallinity, composition, and functional groups.
- 4. To obtain data about the characteristics of synthesized zeolite-A including crystallinity and surface morphology.
- 5. To obtain chemical composition of BCO from pyrolysis of POME.

1.3. Research Benefits

The benefit of this research is as follows:

- 1. To increase the added value of POME as bio gasoline, and pumice as a source of silica for the manufacture of zeolites.
- 2. To overcome the reliance of fossil fuels by increasing the availability of liquid fuel from biomass.

II. LITERATURE REVIEW

2.1. Biomass Pyrolysis

Pyrolysis is a thermal degradation of large organic molecules in a closed reactor, leading to formation of simpler product in the forms of gas, liquid, and solid residue. In the context of renewable energy sources, liquid product of biomass pyrolysis, which is known as biocrude oil (BCO) is of particular interest since this product has the potential to be treated further into practical fuel, such as bio gasoline, bio avtur, and biodiesel.

Pyrolysis is a non-stoichiometry process, however the reactions involved can be distinguished as primary reaction and secondary reaction. Primary reaction are the initial reaction that occur during pyrolysis and involve the direct decomposition of organic materials. Primary reaction of pyrolysis can be classified into several types, including dehydration, decarboxylation, and depolymerization. Secondary reaction of pyrolysis occur after the primary reactions and involve further transformations of the intermediate products formed during pyrolysis, and includes condensation, cracking, and polymerization (Patwardhan *et al.*, 2011).

Since pyrolysis is thermal process, based on the temperature applied, pyrolysis is divided into three schemes known as slow pyrolysis, fast pyrolysis, and flash pyrolysis. Slow pyrolysis is a gradual heating of organic material at relatively low temperatures and longer residence time. Fast pyrolysis involves rapid heating organic matters at high temperatures, typically in the range of 400 to 600°C. Flash pyrolysis involves rapid heating organic matters at very high temperatures

for an extremely short duration, typically in the range of millisecond or a few seconds resulting in the quick decomposition of the material (Onay and Kockar, 2003).

2.2. Chemical Composition of BCO

As previously stated, the main characteristic of BCO is complex composition of large number and various types of organic compounds. Various studies revealed that chemical composition of BCO is strongly determined by two main factors, which are the feedstock and catalyst used, reflected by the results presented on Table 1.

No.	Feedstock	Catalyst	Chemical constituent	Ref	
1.	Mixed cassava solid waste and rubber seed oil	Zeolite-A	Hydrocarbon (74%), ketone (13%), ester (6%), alcohol (5%), aldehyde (1%), and acid (1%)	(Simanjuntak et al., 2019)	
2.	Sugarcane bagasse and sludge palm oil	yarcane Hydrocarbon (76%), alcohol (13%), ester (8%), and ketone (3%)		(Supriyanto <i>et al.</i> , 2018)	
3.	Palm oil Zeolite-X Hydr (169		Hydrocarbon (77%), acid (16%), and ketone (7%)	(Febriyanti <i>et</i> <i>al.</i> , 2020)	
4.	Poplar wood	Pd/CeTiO ₂	Hydrocarbons (0.4%), acid (9.5%), ketone (3%), aldehydes (5.2%), furan (8.4%), sugar (5.3%), phenol (37.2%), and others (8.6%)	(Lu <i>et al.,</i> 2010)	
5.	Sugarcane bagasse and rubber seed oil	Zeolite-Y	Hydrocarbon (87.91%), gasoline fraction (42.60%), kerosene fraction (43.59%), and residual fraction (1.72%)	(Simanjuntak et al., 2019)	
6.	Palm oil	Zeolite-Y	Hydrocarbon (88.76%), fraction of bio gasoline (52.55%), and fraction of kerosene (36.21%)	(Pandiangan et al., 2021)	

Table 1. Chemical composition of BCO produced from different feedstocks with the use of different catalysts

The results presented on Table 1 indicate that it is necessary to use the right catalyst for specific feedstock in order to optimize the formation of the components of BCO which valuable as fuel. At the same time, using the right catalyst is expected to reduce the formation of unwanted components.

2.3. Zeolite-A

Among hundreds of different types of zeolites, zeolite-A is one of the most widely used because of the small aperture of about 4 Å, and high molar ratio of aluminium to silicon (~1), which provides a large number of sites for cation exchange (Ren *et al.*, 2018). Chemical formula of zeolite-A is Na₂O.Al₂O₃.2SiO₂.4,5H₂O, with Na₁₂(AlO₂)₁₂·nH₂O as unit cell. Zeolite-A has the structure consists of interconnected cages or channels that can selectively adsorb and desorb molecules based on their size and polarity. The outstanding characteristics of zeolite-A, including non – toxic and high thermal stability, making zeolite-A extensively used for waste treatment and suitable for applications such as ion exchange, gas separation, and catalysis. Zeolite-A is usually carried out under hydrothermal conditions with a reactive gel base in an alkaline medium at a temperature of 80-200°C. Hydrothermal conditions can be achieved with conventional methods by using oven, bath, or autoclave as the heat source (Wuntu and Tangkuman, 2008). According to Golbad *et al.*, (2017), the framework of zeolite-A is shown on Figure 1.



Figure 1. The LTA framework type (Golbad *et al.*, 2017).

2.4. Pumice Silica

Pumice is a porous volcanic rock contains significant proportions for silica (SiO₂) and alumina (Al₂O₃), and a little amount of metal. Pumice is widely utilized as an alternate feedstocks or mixtures at the industry, for the example is as a source of silica in the manufacture of synthetic zeolite (Mahaddilla and Putra, 2013), because it has the same value and efficiency with high cost adsorbent, such as active carbon and chitosan, and its low in cost is the same as gel silicas. Pumice has percentage of SiO₂ and Al₂O of 48% and 14.9, and Ersoy *et al.* (2010) also stated that pumice is also contains SiO₂ and Al₂O₃ of 70.21% and 13.63% respectively. There are also other components contained, such as MgO, Na₂O, CaO, Fe₂O₃, K₂O, etc.

There are several ways to obtain pure silica from pumice, one of them is through extraction method. This method is done to separate the solute between two insoluble liquids. Influential parameters affecting extraction process namely are temperature, stirring, solvent solution concentration, and extraction time. Basic principle of extraction is by dissolving polar compounds in polar solvents and non-polar compounds in non-polar solvents (Zhang *et al.*, 2018).

2.5. Characterization of Pumice Silica

Pumice silica was characterized using XRD to analyze the crystallographic structure of the sample, either amorphous or crystalline. XRF characterization was done to determine the elemental composition of materials, and FTIR characterization was done to identify the functional groups.

2.5.1. X-Ray Diffraction (XRD)

The basic principle of XRD characterization is based on the catalyst crystal reflects the X-rays sent from the source and received by the detector. Every compounds consist of arrangement of atoms forming a certain plane. In XRD, the diffraction pattern is defined by the size of the angle formed as a result of the light

beam's diffraction by the crystal in the material. The value of the angle is expressed in 2 θ , where θ represents the coming of light, and 2 θ is the angle of incidence with the diffraction angle detected by the detector. Diffraction will only happened if the constructive interference of wave have been formed when the light beam is reflected by the sample material. Meanwhile, the constructive interference will only happened on particular wavelength that comes from particular angle. It means not all wavelengths come from a certain angle will form constructive interference. According to Mourhly *et al.* (2015), the diffractograms of pumice and pumice silica are shown on Figure 2.



Figure 2. Diffractograms of pumice and pumice silica (Mourhly et al., 2015).

2.5.2. X-Ray Fluorescence (XRF)

XRF characterization is an analytical technique to determine elemental composition. The basic principle of XRF is when a primary X-ray that typically generated in a X-ray tube hits the inner shell electron of the atom and ejects the electron. X-ray analyser determines the chemical components contained in the sample by measuring the fluorescent (or secondary) X-rays emitted from the sample when excited by a primary X-ray source. Sample is then irradiated by high energy X-rays from a controlled X-ray tube. When the atom is exposed to X-rays of sufficient energy, electrons from one of the orbital shells of the atom are released. The atoms will regain stability, filling the vacancy remains in the inner shell orbital with electrons from one of the higher energy shell orbitals of the

atom. Electrons then descend to a lower energy level by releasing fluorescence X-rays. The energy of this X-rays is equal to the specific energy difference between the two quantum states of the electron. According to Mourhly *et al.* (2015), chemical composition of pumice determined by XRF is shown on Table 2.

 Table 2. Chemical composition of pumice

Oxide	SiO ₂	Al ₂ O ₃	MgO	Na ₂ O	CaO	Fe ₂ O ₃	K2O	Others
Pumice (%)	14.9	8.34	8.34	8.18	5.70	6.71	1.84	6.33

2.5.3. Fourier Transform Infrared Spectroscopy (FTIR)

The Infrared Fourier Transform is equipped with infrared spectroscopy with the Fourier transform for detection and analysis of the spectrum results. Infrared spectroscopy has benefits for identification of organic compounds because of its complex spectrum, a complex spectrum due to consisting too many peaks indicating the presence of a functional group which indicated by the wave number. According to Ersoy *et al.* (2010), the FTIR spectrum of pumice is shown on Figure 3. The analysis of FTIR was carried out by using Perkin Elmer Spectrum BX-2 and having a standard mid-IR DTGS detector. The IR spectrum of pumice silica is shown on Figure 3.



Figure 3. FTIR spectrum of pumice (Ersoy et al., 2010).

2.6. Characterization of Zeolite-A

Zeolite-A characterization was done using XRD to analyze the crystalline materials of synthesized zeolite-A, and SEM characterization was done to identify the surface morphology of zeolite-A.

2.6.1. X-Ray Diffraction (XRD)

XRD is an analytical method utilizes interaction between x-ray with a beam of atoms arranged in a system of crystals. XRD was done to find out the crystal phase and amorph qualitative and quantitatively, along with its crystallinity percentage from the catalyst. Based on the previous study reported by Simanjuntak *et al.* (2021), diffractograms of zeolite-A are displayed on Figure 4.



Figure 4. Diffractograms of (a) commercial Zeolite-A and synthesized zeolite-A with different calcination time, (b) 48 h, (c) 72 h, and (d) 96 h (Simanjuntak *et al.*, 2021).

2.6.2. Scanning Electron Microscopy (SEM)

Scanning Electron Microscopy (SEM) is one kind of electron microscope used to observe and analyse the surface morphology of crystals. The working principle of SEM is a source electron from the filament made from tungsten emits a beam of light. If the electron is reacting with the specimen, it will produce primary and secondary electron.

Scanning electron microscopy (SEM), also known as SEM analysis or SEM technique is an effective method in the analysis of organic and inorganic materials at the nanometre to micrometre (μ m) scale. SEM works at high magnifications of up to 300.000x and even 1.000.000x to produce very precise images of a wide range of materials. Materials that can be used in SEM are organic and solid inorganic materials including metals and polymers. Figure 5 shows the morphology of zeolite-A from the previous study (Simanjuntak *et al.*, 2021).



Figure 5. Scanning electron microscope (SEM) of zeolite-A (Simanjuntak *et al.*, 2021).

2.7. Liquid Fuel Analysis

Gas Chromatography Mass Spectometry (GC-MS) is used to identify chemical compounds in a mixture of a sample based on the separation of components in a sample mixture on GC and based on fragmentation of compounds on MS come from the GC separation. Working principle of GC-MS is charged gas molecules will be selected according to its mass and weight, spectrum obtained from converting sample into moving ions, then separated based on mass to charge ratio (m/e). Ionization produces fragments which will produce a spectrum. Mass spectrum is a picture between relative abundance with mass to charge ratio (m/e). Chromatogram and chemical compositions of liquid fuel reported by the previous study is shown on Figure 6.



Figure 6. Chromatogram and Relative Composition of Liquid Fuel (Simanjuntak *et al.*, 2019).

III. RESEARCH METHOD

3.1. Place and Time of Research

This research has been done at the Polymer Laboratory, Department of Chemistry, Faculty of Mathematics and Natural Sciences, University of Lampung in October 2022 – March 2023. XRD analysis was carried out at ITS Surabaya, SEM analysis was carried out at UPT LTSIT University of Lampung, XRF analysis was carried out at Universitas Negeri Padang, FTIR analysis was carried out at Diponegoro University, and GC-MS analysis was carried out at Gadjah Mada University Yogyakarta and Poltekkes Bandung.

3.2. Tools and Materials

3.2.1. Tools

Tools used in this research are included; pyrolysis device, stove, lock and lock container, plate, furnace, teflon, spatula, 300 mesh, plastic jar, analytical balance, filter, pestle and mortar, bucket, oven, hotplate stirrer, magnetic stirrer, glass wares, scanning electron microscope model ZEISS EVO MA 10 for SEM, PANalytical type empyrean diffractometer for XRD, PANalytical Epsilon 3 for X-Ray Fluorescence XRF, Perkin Elmer for FTIR, and QP2010S SHIMADZU for GC-MS.

3.2.2. Materials

Materials used in this research were included; POME, pumice, food grade aluminium foil, solid NaOH, 3 M of HNO3 solution, 2.5 M of NaOH solution, 1 M of HCl solution, distilled water, filter paper, universal pH paper, and heat exchanger.

3.3. Research Procedures

This research consists following procedures; (1) pumice preparation, (2) pumice extraction, (3) synthesize of zeolite-A, (4) zeolite-A characterization, (5) liquid fuel manufacture, and (6) liquid fuel analysis.

3.3.1. Pumice Preparation

In this research, pumice was washed with water then sun dried for a day, and finally oven dried at 100°C overnight. Cleaned and dried pumice was then mashed into powder using pestle and mortar, and then sieved using 200 mesh to obtain sample with homogeneous size. To remove non-silica components, the pumice powder was soaked in HCl solution 1 M for 24 hours, then rinsed with distilled water to remove acid, and oven dried at 100°C for a night.

3.3.2. Pumice Extraction

To conduct extraction, a mass of 40 g pumice powder was mixed with NaOH solution and the mixture was stirred for 24 hours at 100°C. The sample was filtered and the filtrate was neutralized using 3 M of HNO₃ solution to produce silica gel. The resulting gel was aged for 4 hours then washed with hot water and finally oven dried for a night at 100°C. Solid silica formed was ground then sieved with 200 mesh to obtain silica powder. Silica powder obtained was then characterized by using XRD, XRF, and FTIR.

3.3.3. Synthesis of Zeolite-A

Synthesis of zeolite-A was carried out by dissolving 22.32 g of NaOH pellets in various amount of distilled water; 150, 200, 250, and 430 mL. Then divide the NaOH solution into two, one was to dissolve 13.32 g of aluminium foil to produce sodium aluminate and the other one was to be dissolved with 20 g of pumice silica to prepare sodium silicate. To produce the precursor of zeolite, both mixtures were stirred for 3 hours. Natrium aluminate produced then put in the autoclave for 24 hours then crystallized in the oven for 72 hours at 100°C. Then sample was washed and oven dried at 100°C to produce dry solid. Powder sample prepared

by ground the solid and calcined at various temperatures of 600, 700, and 800°C for 6 hours. Zeolite-A obtained then characterized by using XRD and SEM.

3.3.4. Zeolite-A Characterization

Zeolite-A characterization was done using XRD and SEM. XRD characterization was conducted to identify the crystal phase of the sample, and SEM characterization was conducted to analyze the surface morphology of the sample.

3.3.4.1. X-Ray Diffraction (XRD)

XRD analysis was carried out using PANalytical with Cu anode material, 40 kV energy and 30 mA current, and diffraction angle in the range of $5 - 50^{\circ}$ to identify the XRD pattern. XRD data obtained were analyzed using Match!3 software Ver. 2.4.7 build 529 and data were compared to standard data available on International Zeolite Association (IZA).

3.3.4.2. Scanning Electron Microscope (SEM)

SEM analysis was carried out using SEM ZEISS EVO MA 10 with the instrument electron acceleration voltage at 15.00 kV, the window (WD) of 8.5 and 9.5 mm, magnification (Mag) up to 35.000 times.

3.3.5. Liquid Fuel Manufacture

In this research, pyrolysis was conducted in 5 variables, which are regular pyrolysis, using heat exchanger, and using various calcined temperature of zeolite-A (Sample E – G). Regular pyrolysis and pyrolysis using heat exchanger have the same method, but the addition of silica sand as heat exchanger was mandatory for pyrolysis using heat exchanger. An amount of 500 mL of POME was pyrolyzed in a laboratory scale up to 3 hours with low heat.

About 20 minutes after the preheating, the first drop of BCO was dripped and collected in a glass bottle. Pyrolysis was done for about 3 hours or until no BCO was dripping and 209 mL of BCO was produced. BCO produced then filtered by using filter paper to separate it from impurities, then kept overnight in a separatory funnel to separate the organic and inorganic phase. Afterwards, the

organic phase of BCO was characterized with GC-MS to identify the components contained in the sample.

BCO produced with catalytic upgrading was carried out by using 5 g of synthesized zeolite-A into 100 mL of POME BCO and put into the pyrolysis reactor. Catalytic upgrading pyrolysis was taken up to 30 minutes and liquid fuel obtained were put into the separatory funnel to separate the organic phase (BCO) and inorganic phase. BCO was characterized using GC-MS to analyse the chemical components in the sample.

3.3.6. Liquid Fuel Analysis

Liquid fuel characterization was carried out by using the GC-MS type QP2010S Shimadzu to identify the components in the sample with column type Rtx 5 (30 m length; ID 0.25 mm; film thickness: 0.25 m; carrier gas: Helium; EI 70 Ex). The injector temperature was 310°C with split mode, the detector temperature was 250°C, the oven column temperature was 40°C, the flow rate at a pressure of 13 kPa and a total flow of 80 mL.min⁻¹. The standard used for the characterization of liquid fuel is by using the GC-MS standard.

V. CONCLUSIONS AND SUGGESTIONS

5.1. Conclusions

Based on the experimental results, it can be concluded that:

- Amorphous pumice silica has been successfully extracted with 2.5 M of NaOH solution.
- Zeolite-A has been successfully synthesized using 1.29 M of NaOH solution with hydrothermal method by an addition of food grade aluminium foil with Si/Al ratio 1.
- 3. BCO produced with zeolite-A 700 has the highest hydrocarbon contained in the sample with relative percentage 84%, while BCO produced with heat exchanger has the least amount with relative percentage of 67.86%.
- 4. BCO produced with regular pyrolysis has the highest bio gasoline content with relative percentage 54% and BCO produced with heat exchanger has the least amount with relative percentage of 25%.

4.2. Suggestions

Based on the results obtained, the following studies are suggested.

- 1. To use lower concentration of NaOH to form zeolite-A with higher crystalline phase.
- 2. Further investigation for catalytic upgrading of the BCO to increase the biogasoline content.

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